

### Problem 1.3-10

A current of 100 amps passes through a bare stainless-steel wire of  $D = 1.0$  mm diameter. The thermal conductivity and electrical resistance per unit length of the wire are  $k = 15$  W/m-K and  $R'_e = 0.14$  ohm/m, respectively. The wire is submerged in an oil that is maintained at  $T_\infty = 30^\circ\text{C}$ . The steady-state temperature at the center of the wire is measured to be  $180^\circ\text{C}$ , independent of axial position within the oil bath.

a) What is the temperature at the outer surface of the wire?

The inputs are entered in EES:

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$UnitSystem SI MASS RAD PA K J
$TABSTOPS 0.2 0.4 0.6 0.8 3.5 in

k=15 [W/m-K]
R\L=0.14 [ohm/m]
i=100 [amp]
D=1[mm]/2*convert(mm,m)
T_c=converttemp(C,K,180 [C])
T_oil=converttemp(C,K,30 [C])
L=1 [m]
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"conductivity of wire"  
"resistance per unit length of wire"  
"current"  
"diameter"  
"temperature at center of wire"  
"temperature of oil"  
"per unit length basis"

The rate of generation per unit volume is:

$$\dot{g}''' = \frac{I^2 R'_e L}{L \pi r_{out}^2} \quad (1)$$

where  $r_{out}$  is the outer radius of the wire:

$$r_{out} = \frac{D}{2} \quad (2)$$

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r_out=D/2
g_dot'''*(pi*r_out^2*L)=i^2*R\L*L
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"outer radius"  
"rate of volumetric generation"

The general solution for radial conduction with uniform volumetric generation is provided in Table 1-3:

$$T = -\frac{\dot{g}''' r^2}{4k} + C_1 \ln(r) + C_2 \quad (3)$$

$$\frac{dT}{dr} = -\frac{\dot{g}''' r}{2k} + \frac{C_1}{r} \quad (4)$$

In order for the temperature to remain bounded at  $r = 0$ , it is necessary that  $C_1$  be zero. The temperature at the center is therefore:

$$T_c = C_2 \quad (5)$$

T\_c=C\_2 "solve for C\_2"

The temperature at the surface is given by:

$$T_s = -\frac{\dot{g}''' r_{out}^2}{4k} + C_1 \ln(r_{out}) + C_2 \quad (6)$$

T\_s=-g\_dot'''\*r\_out^2/(4\*k)+C\_2 "surface temperature"  
T\_s\_C=converttemp(K,C,T\_s) "in C"

which leads to  $T_s = 172.6^\circ\text{C}$ .

b) Estimate the convection coefficient between the submerged wire and the oil.

An interface energy balance at  $r = r_{out}$  leads to:

$$\bar{h}(T_{oil} - T_s) = k \left. \frac{dT}{dr} \right|_{r=r_{out}} \quad (7)$$

where the temperature gradient is evaluated using Eq. (4):

$$\left. \frac{dT}{dr} \right|_{r=r_{out}} = -\frac{\dot{g}''' r_{out}}{2k} \quad (8)$$

dT/dr\_s=-g\_dot'''\*r\_out/(2\*k) "surface temperature gradient"  
h\_bar\*(T\_oil-T\_s)=k\*dT/dr\_s "interface energy balance"

which leads to  $\bar{h} = 6250 \text{ W/m}^2\text{-K}$ .

c) A plastic material ( $k_p = 0.05 \text{ W/m-K}$ ) can be applied to the outer surface of the wire. Can the insulation result in a reduction of the center temperature? If so, what insulation thickness should be applied?

The resistance to conduction through the insulation is:

$$R_{ins} = \frac{\ln\left(\frac{r_{out} + th_{ins}}{r_{out}}\right)}{2\pi k_p L} \quad (9)$$

and the resistance to convection from the surface of the insulation is:

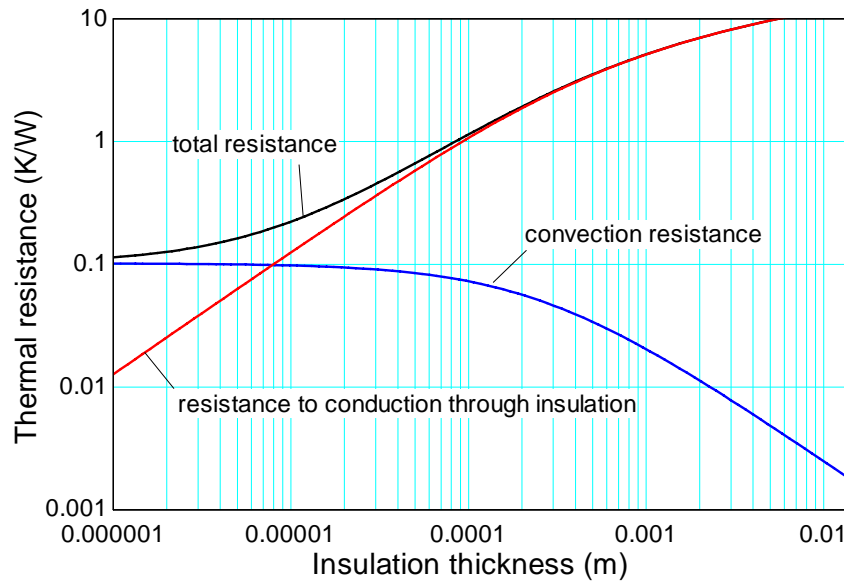
$$R_{conv} = \frac{1}{2\pi r_{out} L \bar{h}} \quad (10)$$

The total resistance between the surface of the wire and the oil is:

$$R_{total} = R_{conv} + R_{ins} \quad (11)$$

k_p=0.05 [W/m-K]	"conductivity of plastic"
R_ins=ln((r_out+th_ins)/r_out)/(2*pi*k_p*L)	"resistance to conduction through plastic"
R_conv=1/(h_bar*2*pi*L*(r_out+th_ins))	"resistance to convection from external surface"
R_total=R_ins+R_conv	"total resistance from surface of wire"

Figure 1 illustrates  $R_{ins}$ ,  $R_{conv}$ , and  $R_{total}$  as a function of the insulation thickness. Notice that increasing the insulation thickness reduces  $R_{conv}$  because there is more surface area for convection but increases  $R_{cond}$  because the length for conduction is longer. In some situations, the reduction in  $R_{conv}$  dominates the problem and therefore the total resistance may be reduced by adding insulation. However, in this case, there is no such region.



**Figure 5: Resistance to convection, resistance to conduction through insulation, and total resistance from wire surface as a function of the insulation thickness.**